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Oppg 2a)

$$S_{DU_1} = \frac{\Gamma_D}{\Gamma_U} = \frac{800 \exp\left(\frac{-2000}{T}\right) C_A^{0,5} C_C}{10 \exp\left(\frac{-300}{T}\right) C_A C_C}$$

$$S_{DU_1} = 80 \exp\left(\frac{-1700}{T}\right) C_A^{-0,5}$$

S_{DU_1} er høy ved høy T og lav C_A .

Oppg 2a)

$$\Gamma_{1A} = -k_{1A} C_A = -0,07 \frac{\text{mol}}{\text{L min}}$$

$$\Gamma_{2A} = -\frac{1}{3} \Gamma_{2D} = -2,6 \cdot 10^{-3} \frac{\text{mol}}{\text{L min}}$$

$$\Gamma_{3A} = 0$$

$$\Gamma_{1B} = -\frac{1}{3} \Gamma_{1A} = 0,023 \frac{\text{mol}}{\text{L min}}$$

$$\Gamma_{2B} = \Gamma_{3B} = 0$$

$$\Gamma_{1C} = \Gamma_{1B} = 0,023 \frac{\text{mol}}{\text{L min}}$$

$$\Gamma_{2C} = 2 \Gamma_{2A} = -5,2 \cdot 10^{-3} \frac{\text{mol}}{\text{L min}}$$

$$\Gamma_{3C} = -\Gamma_{3E} = -5 \cdot 10^{-4} \frac{\text{mol}}{\text{L min}}$$

$$\Gamma_A = \sum \Gamma_{iA} = -0,0726 \frac{\text{mol}}{\text{L min}}$$

$$\Gamma_B = 0,023 \frac{\text{mol}}{\text{L min}}$$

$$\Gamma_C = 0,0173 \frac{\text{mol}}{\text{L min}}$$

Oppg 2e)

$$r_A = -0,0726 \frac{\text{mol}}{\text{L} \cdot \text{min}}$$

$$\left. \begin{array}{l} V_T = V_{\text{IN}} + V_{\text{DAKKET}} \\ F_A - F_{A0} - r_A V = 0 \end{array} \right\} \rightarrow \text{Fordi: Steadystate}$$

$$V = \frac{F_A - F_{A0}}{r_A} = \frac{\Phi_V (C_A - C_{A0})}{r_A}$$

* for væskefase
er $\Phi_V = \Phi_{V0}$

$$V = 3995 \text{ L} \approx 4 \text{ m}^3$$

Oppg 3a)

$$C_{A0} = 3,2 \frac{\text{mol}}{\text{L}}, F_{B0} = 5 F_{A0}$$

$$k(31^\circ\text{C}) = 150 \cdot 10^{-3} \frac{\text{L}}{\text{mol} \cdot \text{h}}$$



	T_i sett	dakket	etter reaksjon
A:	$\Phi_V C_{A0}$	$-r_A V$	$\Phi_V C_{A0} - r_A V$
B:	$5\Phi_V C_{A0}$	$-r_A V$	$5\Phi_V C_{A0} - r_A V$
C:	0	$r_A V$	$r_A V$
D:	0	$r_A V$	$r_A V$

$$3b) r_{Cn} = 20 \frac{\text{kmol}}{\text{h}}, V_{rx} = 4000 \text{ L}, T = 31^\circ\text{C}$$

$$\text{I) } r_A = -r_C \quad \text{III) } C_A = \frac{\Phi_V C_{A0} - r_A V}{\Phi_V}$$

$$\text{II) } -r_A = k C_A C_B \quad \text{IV) } C_B = \frac{5\Phi_V C_{A0} - r_A V}{\Phi_V}$$

$$\text{V) } X_A = \frac{F_{A0} - F_A}{F_{A0}} = \frac{C_{A0} - C_A}{C_{A0}}$$

* for væskefase / Steadystate

$$\tilde{r} = \frac{V}{\Phi_V}$$

$$(\text{III, IV}) \rightarrow \text{II} \rightarrow \text{I: VI) } r_C = k(C_{A0} - r_A \tilde{r})(5C_{A0} - r_A \tilde{r})$$

$$\tilde{r} = 3,16 \text{ min}$$

$$\rightarrow C_A = 0,04 \frac{\text{mol}}{\text{L}} \rightarrow X = 0,98$$